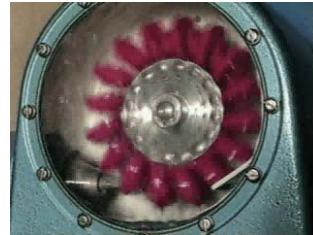


Finite Control Volume Analysis



Moving from a System to a Finite Control Volume



• Mass



• Linear Momentum



• Moment of Momentum



• Energy

• Putting it all together!

Conservation of Mass



B = Total amount of mass in the system

b = mass per unit mass = 1

$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \int_{cv} \rho b dV + \int_{cs} \rho b \mathbf{V} \cdot \hat{\mathbf{n}} dA \quad \text{cv equation}$$

$$\frac{DM_{sys}}{Dt} = \frac{\partial}{\partial t} \int_{cv} \rho dV + \int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA \quad \text{But } DM_{sys}/Dt = 0!$$

$$\int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial}{\partial t} \int_{cv} \rho dV \quad \text{Continuity Equation}$$

mass leaving - mass entering = - rate of increase of mass in cv

Conservation of Mass

$$\int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial}{\partial t} \int_{cv} \rho dV \quad \text{If mass in cv is constant}$$

$$\int_{cs_1} \rho_1 \mathbf{V}_1 \cdot \hat{\mathbf{n}}_1 dA + \int_{cs_2} \rho_2 \mathbf{V}_2 \cdot \hat{\mathbf{n}}_2 dA = 0$$

$$\int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = \rho \bar{V} A = \dot{m} \quad [\text{M/T}]$$

$$\bar{V} = \frac{\int_{cs} \mathbf{V} \cdot \hat{\mathbf{n}} dA}{A}$$

Unit vector $\hat{\mathbf{n}}$ is normal to surface and pointed out of cv

We assumed uniform ρ on the control surface

$\bar{V}$ is the spatially averaged

Continuity Equation for Constant Density and Uniform Velocity

$$\int_{cs_1} \rho_1 \mathbf{V}_1 \cdot \hat{\mathbf{n}}_1 dA + \int_{cs_2} \rho_2 \mathbf{V}_2 \cdot \hat{\mathbf{n}}_2 dA = 0$$

$$-\rho_1 \bar{V}_1 A_1 + \rho_2 \bar{V}_2 A_2 = 0 \quad \text{Density is constant across cs}$$

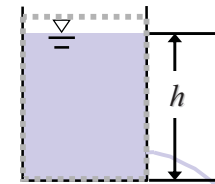
$$\bar{V}_1 A_1 = \bar{V}_2 A_2 = Q \quad [\text{L}^3/\text{T}] \quad \text{Density is the same at } cs_1 \text{ and } cs_2$$

$$V_1 A_1 = V_2 A_2 = Q$$

Simple version of the continuity equation for conditions of constant density. It is understood that the velocities are either uniform or spatially averaged.

Example: Conservation of Mass?

The flow out of a reservoir is 2 L/s.
The reservoir surface is 5 m x 5 m.
How fast is the reservoir surface dropping?



$$\int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial}{\partial t} \int_{cv} \rho dV$$

$$\int_{cs} \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial V}{\partial t}$$

Constant density

$$Q_{out} - Q_{in} = - \frac{dV}{dt}$$

$$Q_{out} = - \frac{A_{res} dh}{dt}$$

Velocity of the reservoir surface

$$\left(\frac{dh}{dt} \right) = - \frac{Q}{A_{res}}$$

Example: Conservation of Mass

- The flow through the orifice is a function of the depth of water in the reservoir $Q = CA_o \sqrt{2gh}$
- Find the time for the reservoir level to drop from 10 cm to 5 cm. The reservoir surface is 15 cm x 15 cm. The orifice is 2 mm in diameter and is 2 cm off the bottom of the reservoir. The orifice coefficient is 0.6.
- CV with constant or changing mass.
- Draw CV, label CS, solve using variables starting with

$$\int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial}{\partial t} \int_{cv} \rho dV$$

Example Conservation of Mass Constant Volume

$$\int_{cs} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial}{\partial t} \int_{cv} \rho dV$$

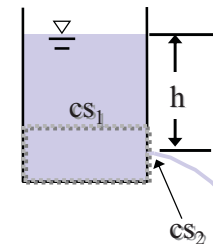
$$\int_{cs_1} \rho_1 \mathbf{V}_1 \cdot \hat{\mathbf{n}}_1 dA + \int_{cs_2} \rho_2 \mathbf{V}_2 \cdot \hat{\mathbf{n}}_2 dA = 0$$

$$-V_{res} A_{res} + V_{or} A_{or} = 0$$

$$V_{or} A_{or} = Q_{or}$$

$$V_{res} = \frac{-dh}{dt}$$

$$\frac{dh}{dt} A_{res} + CA_{or} \sqrt{2gh} = 0$$



Example Conservation of Mass Changing Volume

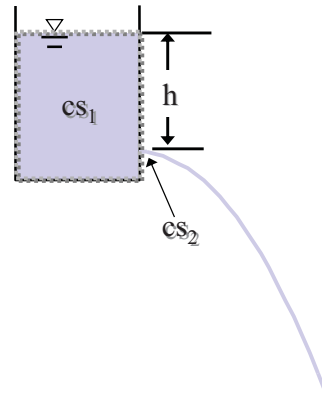
$$\int_{CS} \rho \mathbf{V} \cdot \hat{\mathbf{n}} dA = - \frac{\partial}{\partial t} \int_{CV} \rho dV$$

$$V_{or} A_{or} = - \frac{\partial}{\partial t} \int_{CV} dV$$

$$V_{or} A_{or} = - \frac{dV}{dt} = - \frac{A_{res} dh}{dt}$$

$$V_{or} A_{or} = Q_{or}$$

$$\frac{dh}{dt} A_{res} + CA_{or} \sqrt{2gh} = 0$$



Example Conservation of Mass

$$\frac{-A_{res}}{CA_{or} \sqrt{2g}} \int_{h_0}^h \frac{dh}{\sqrt{h}} = \int_0^t dt$$

$$\frac{-A_{res}}{CA_{or} \sqrt{2g}} 2(h^{1/2} - h_0^{1/2}) = t$$

$$\frac{-2(0.15\text{ m})^2}{(0.6) \left(\frac{\pi (0.002\text{ m})^2}{4} \right) \sqrt{2(9.8\text{ m/s}^2)}} ((0.03\text{ m})^{1/2} - (0.08\text{ m})^{1/2}) = t$$

$$t = 591\text{ s}$$

Linear Momentum Equation



$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \int_{CV} \rho b dV + \int_{CS} \rho b \mathbf{V} \cdot \hat{\mathbf{n}} dA \quad \text{R.T.T.} \quad \sum \mathbf{F} \neq 0$$

$$\mathbf{B} = m \mathbf{V} \quad \text{momentum} \quad \mathbf{b} = \frac{m \mathbf{V}}{m} \quad \text{momentum/unit mass}$$

$$\frac{Dm \mathbf{V}}{Dt} = \frac{\partial}{\partial t} \int_{CV} \rho \mathbf{V} dV + \int_{CS} \rho \mathbf{V} \mathbf{V} \cdot \hat{\mathbf{n}} dA$$

$$\frac{Dm \mathbf{V}}{Dt} = \int_{CS} \rho \mathbf{V} \mathbf{V} \cdot \hat{\mathbf{n}} dA \quad \text{Steady state}$$

Linear Momentum Equation

$$\frac{Dm \mathbf{V}}{Dt} = \int_{CS} \rho \mathbf{V} \mathbf{V} \cdot \hat{\mathbf{n}} dA$$

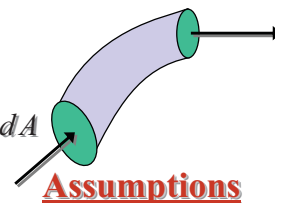
$$\frac{Dm \mathbf{V}}{Dt} = \int_{CS_1} \rho_1 \mathbf{V}_1 \mathbf{V}_1 \cdot \hat{\mathbf{n}}_1 dA + \int_{CS_2} \rho_2 \mathbf{V}_2 \mathbf{V}_2 \cdot \hat{\mathbf{n}}_2 dA$$

$$\frac{Dm \mathbf{V}}{Dt} = -(\rho_1 V_1 A_1) \underline{\underline{\mathbf{V}}_1} + (\rho_2 V_2 A_2) \underline{\underline{\mathbf{V}}_2}$$

$$\underline{\underline{\mathbf{M}}}_1 = -(\rho_1 V_1 A_1) \underline{\underline{\mathbf{V}}_1} = -(\rho Q) \underline{\underline{\mathbf{V}}_1}$$

$$\underline{\underline{\mathbf{M}}}_2 = (\rho_2 V_2 A_2) \underline{\underline{\mathbf{V}}_2} = (\rho Q) \underline{\underline{\mathbf{V}}_2}$$

Vectors!!!



Assumptions

- Uniform density
- Uniform velocity
- $\mathbf{V} \perp \mathbf{A}$
- Steady
- $\mathbf{V}$ fluid velocity

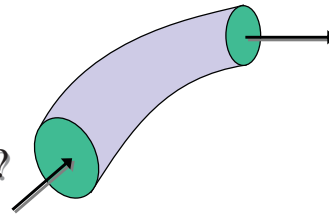
Steady Control Volume Form of Newton's Second Law

$$\sum \mathbf{F} = \frac{D(m\mathbf{V})}{Dt} = \mathbf{M}_1 + \mathbf{M}_2$$

- What are the forces **acting on the fluid** in the control volume?

- Gravity
- Shear forces at the walls
- Pressure forces at the walls
- Pressure forces on the ends

$$\sum \mathbf{F} = \mathbf{W} + \mathbf{F}_{p_1} + \mathbf{F}_{p_2} + \mathbf{F}_{p_{wall}} + \mathbf{F}_{\tau_{wall}}$$



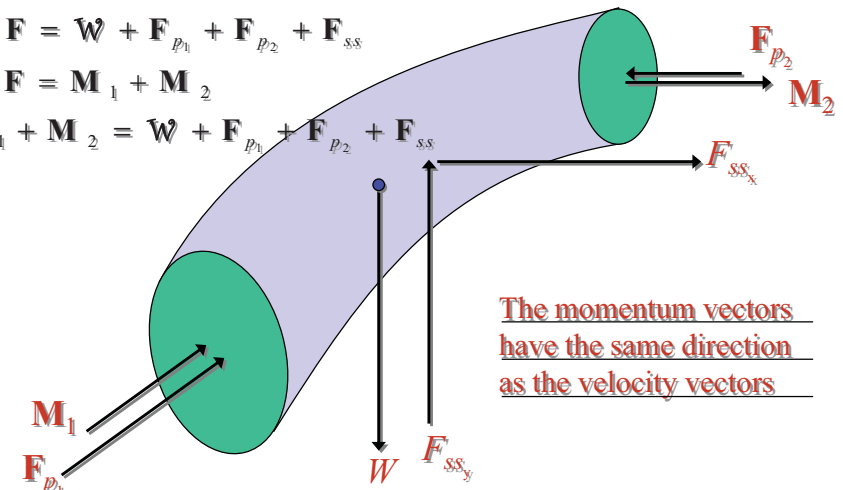
$$\sum \mathbf{F} = \mathbf{M}_1 + \mathbf{M}_2$$

Linear Momentum Equation

$$\sum \mathbf{F} = \mathbf{W} + \mathbf{F}_{p_1} + \mathbf{F}_{p_2} + \mathbf{F}_{ss}$$

$$\sum \mathbf{F} = \mathbf{M}_1 + \mathbf{M}_2$$

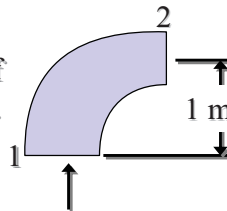
$$\mathbf{M}_1 + \mathbf{M}_2 = \mathbf{W} + \mathbf{F}_{p_1} + \mathbf{F}_{p_2} + \mathbf{F}_{ss}$$



Example: Reducing Elbow

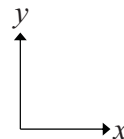
Reducing elbow in vertical plane with water flow of 300 L/s. The volume of water in the elbow is 200 L. Energy loss is negligible. $P_1 = 150$ kPa. Calculate the force of the elbow on the fluid.

$$\mathbf{W} = -1961 \text{ N} \uparrow$$



$$\text{section 1} \quad \text{section 2} \quad \mathbf{M}_1 + \mathbf{M}_2 = \mathbf{W} + \mathbf{F}_{p_1} + \mathbf{F}_{p_2} + \mathbf{F}_{ss}$$

D	50 cm	30 cm	
A	0.196 m^2	0.071 m^2	
V	$1.53 \text{ m/s} \uparrow$	$4.23 \text{ m/s} \rightarrow$	
p	150 kPa	?	
$\mathbf{M}$	$-459 \text{ N} \uparrow$	$1269 \text{ N} \rightarrow$	Direction of V vectors
F_p	$29,400 \text{ N} \uparrow$	?	



Example: What is p_2 ?

$$\frac{p_1}{\gamma_1} + z_1 + \frac{V_1^2}{2g} = \frac{p_2}{\gamma_2} + z_2 + \frac{V_2^2}{2g}$$

$$p_2 = p_1 + \gamma \left[z_1 - z_2 + \frac{V_1^2}{2g} - \frac{V_2^2}{2g} \right]$$

$$p_2 = (150 \times 10^3 \text{ Pa}) + (9810 \text{ N/m}^3) \left[0 - 1 \text{ m} + \frac{(1.53 \text{ m/s})^2}{2(9.8 \text{ m/s}^2)} - \frac{(4.23 \text{ m/s})^2}{2(9.8 \text{ m/s}^2)} \right]$$

$$P_2 = 132 \text{ kPa}$$

$$F_{p_2} = -9400 \text{ N}$$

Example: Reducing Elbow Horizontal Forces

$$\mathbf{M}_1 + \mathbf{M}_2 = \mathbf{W} + \mathbf{F}_{p1} + \mathbf{F}_{p2} + \mathbf{F}_{ss}$$

$$\mathbf{F}_{ss} = \mathbf{M}_1 + \mathbf{M}_2 - \mathbf{W} - \mathbf{F}_{p1} - \mathbf{F}_{p2}$$

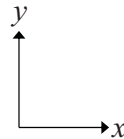
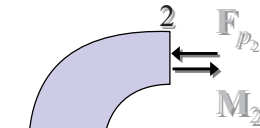
$$F_{ssx} = M_{1x} + M_{2x} - W_x - F_{p1x} - F_{p2x}$$

$$F_{ssx} = M_{2x} - F_{p2x}$$

$$F_{ssx} = (1269 \text{ N}) - (-9400 \text{ N})$$

$$F_{ssx} = 10.7 \text{ kN} \quad \text{Force of pipe on fluid}$$

Pipe wants to move to the left



Example: Reducing Elbow Vertical Forces

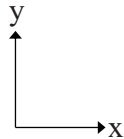
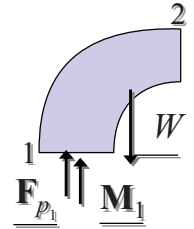
$$F_{ssy} = M_{1y} + M_{2y} - W_y - F_{p1y} - F_{p2y}$$

$$F_{ssy} = M_{1y} - W_y - F_{p1y}$$

$$F_{ssy} = -459 \text{ N} - (-1,961 \text{ N}) - (29,400 \text{ N})$$

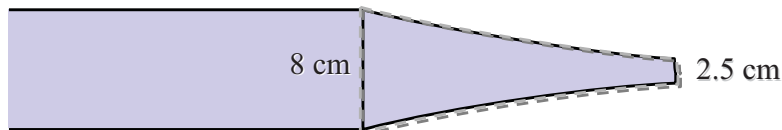
$$F_{ssy} = -27.9 \text{ kN} \quad \underline{28 \text{ kN acting downward on fluid}}$$

Pipe wants to move up



Example: Fire nozzle

A small fire nozzle is used to create a powerful jet to reach far into a blaze. Estimate the force that the water exerts on the fire nozzle. The pressure at section 1 is 1000 kPa (gage). Ignore frictional losses in the nozzle.

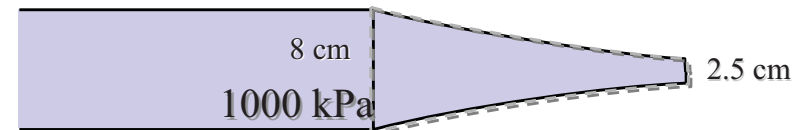


Fire nozzle

Identify what you need to know

Count your unknowns

Determine what equations you will use



Find the Velocities

$$\frac{p_1}{\gamma} + z_1 + \frac{V_1^2}{2g} = \frac{p_2}{\gamma} + z_2 + \frac{V_2^2}{2g}$$

$$\frac{p_1}{\gamma} + \frac{V_1^2}{2g} = \frac{V_2^2}{2g}$$

$$\frac{p_1}{\gamma} = \frac{V_2^2}{2g} - \frac{V_1^2}{2g}$$

$$p_1 = \rho \frac{V_2^2}{2} \left(1 - \left(\frac{D_2}{D_1} \right)^4 \right)$$

$$V_1 D_1^2 = V_2 D_2^2$$

$$V_2^2 \left(\frac{D_2}{D_1} \right)^4 = V_1^2$$

$$V_2 = \sqrt{\frac{2p_1}{\rho \left[1 - \left(\frac{D_2}{D_1} \right)^4 \right]}}$$

Fire nozzle: Solution

	section 1	section 2
D	0.08	0.025 m
A	0.00503	0.00049 m ²
P	1000000	0 Pa
V	4.39	44.94 m/s
F _p	5027	N
M	-96.8	991.2 N
F _{ssx}	-4132	N
Q	22.1	L/s

$$F_{ssx} = M_{1x} + M_{2x} - W_x - F_{p1x} - F_{p2x}$$



Which direction does the nozzle want to go? $\longrightarrow$

Is this the force that the firefighters need to brace against? NO!

force applied by nozzle on water

Example: Momentum with Complex Geometry

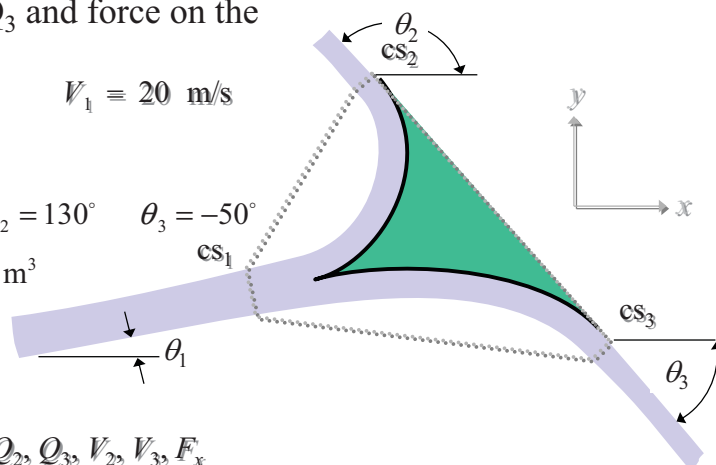
Find Q_2 , Q_3 and force on the wedge.

$$Q_1 = 10 \text{ L/s} \quad V_1 = 20 \text{ m/s}$$

$$F_y = 0$$

$$\theta_1 = 10^\circ \quad \theta_2 = 130^\circ \quad \theta_3 = -50^\circ$$

$$\rho = 1000 \text{ kg/m}^3$$



Unknown: Q_2, Q_3, V_2, V_3, F_x

5 Unknowns: Need 5 Equations

Identify the 5 equations!

Unknowns: Q_2, Q_3, V_2, V_3, F_x

Continuity $Q_1 = Q_2 + Q_3$

Bernoulli (2x)

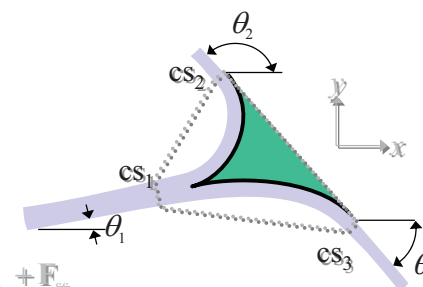
$$\frac{p_1}{\gamma} + z_1 + \frac{V_1^2}{2g} = \frac{p_2}{\gamma} + z_2 + \frac{V_2^2}{2g}$$

$$V_1 = V_2$$

$$V_1 = V_3$$

Momentum (in x and y)

$$M_1 + M_2 + M_3 = W + F_{p1} + F_{p2} + F_{p3} + F_{ss}$$



Solve for Q_2 and Q_3

$$\mathbf{M}_1 + \mathbf{M}_2 + \mathbf{M}_3 = \cancel{W} + \cancel{\mathbf{F}_{p1}} + \cancel{\mathbf{F}_{p2}} + \cancel{\mathbf{F}_{p3}} + \mathbf{F}_{ss} \quad \text{atmospheric pressure}$$

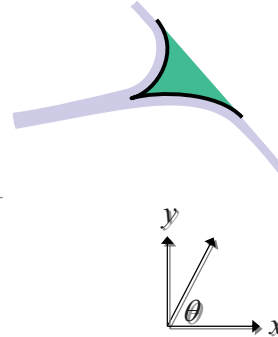
$$F_y = 0 = M_{1y} + M_{2y} + M_{3y}$$

$$0 = -\rho Q_1 V_1 \sin \theta_1 + \rho Q_2 V_2 \sin \theta_2 + \rho Q_3 V_3 \sin \theta_3$$

$$V \sin \theta = \text{Component of velocity in y direction}$$

$$Q_1 = Q_2 + Q_3 \quad \text{Mass conservation}$$

$$V_1 = V_2 = V_3 \quad \text{Negligible losses – apply Bernoulli}$$



Solve for Q_2 and Q_3

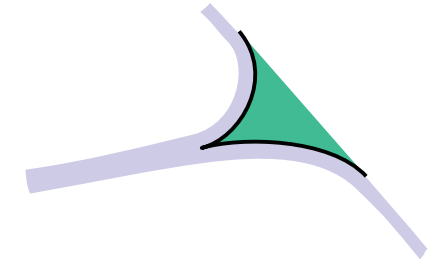
$$0 = \cancel{-\rho Q_1 V_1 \sin \theta_1} + \cancel{\rho Q_2 V_2 \sin \theta_2} + \cancel{\rho Q_3 V_3 \sin \theta_3}$$

$$0 = -Q_1 \sin \theta_1 + Q_2 \sin \theta_2 + Q_3 \sin \theta_3 \quad \underline{Q_3 = Q_1 - Q_2}$$

$$Q_2 = Q_1 \frac{(-\sin \theta_1 + \sin \theta_3)}{(-\sin \theta_2 + \sin \theta_3)}$$

$$Q_2 = 6.133 \text{ L/s}$$

$$Q_2 = Q_1 \frac{[-\sin(10) + \sin(-50)]}{[-\sin(130) + \sin(-50)]}$$



$$Q_3 = 3.867 \text{ L/s}$$

Solve for F_x

$$F_x = M_{1x} + M_{2x} + M_{3x}$$

$$F_x = -\rho Q_1 V_1 \cos \theta_1 + \rho Q_2 V_2 \cos \theta_2 + \rho Q_3 V_3 \cos \theta_3$$

$$F_x = \rho V_1 [-Q_1 \cos \theta_1 + Q_2 \cos \theta_2 + Q_3 \cos \theta_3]$$

$$F_x = (1000 \text{ kg/m}^3)(20 \text{ m/s}) \begin{bmatrix} -(0.01 \text{ m}^3/\text{s})\cos(10) \\ +(0.006133 \text{ m}^3/\text{s})\cos(130) \\ +(0.003867 \text{ m}^3/\text{s})\cos(-50) \end{bmatrix}$$

$$F_x = -226 \text{ N} \quad \text{Force of wedge on fluid}$$

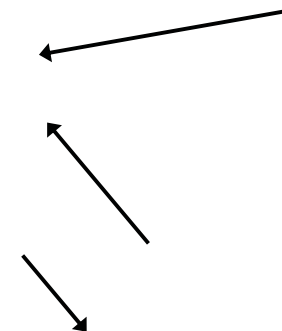
Vector solution

$$\mathbf{M}_1 + \mathbf{M}_2 + \mathbf{M}_3 = \mathbf{F}_{ss}$$

$$|\mathbf{M}_1| = |-\rho Q_1 V_1| = 200 \text{ N}$$

$$|\mathbf{M}_2| = |\rho Q_2 V_2| = 122.66 \text{ N}$$

$$|\mathbf{M}_3| = |\rho Q_3 V_3| = 77.34 \text{ N}$$

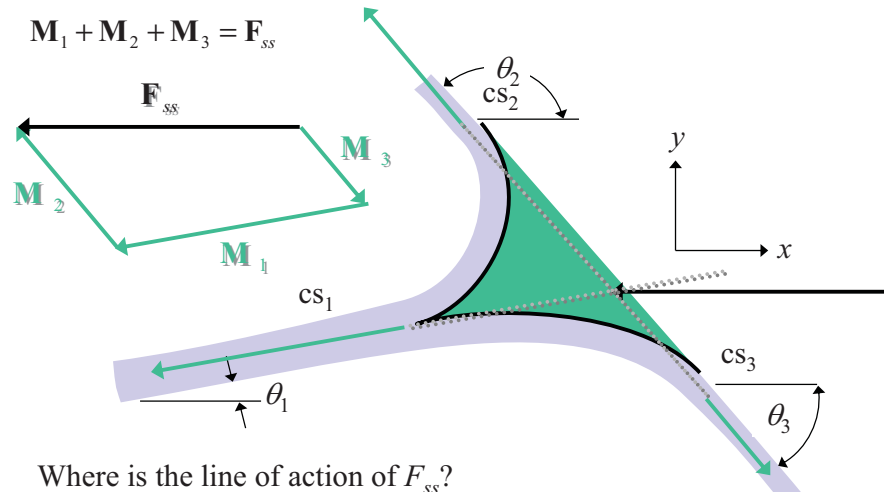


$$Q_2 = 10 \text{ L/s}$$

$$Q_2 = 6.133 \text{ L/s}$$

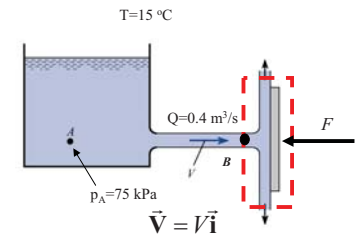
$$Q_3 = 3.867 \text{ L/s}$$

Vector Addition



Example

- **Given:** Figure
- **Find:** Horizontal force required to hold plate in position
- **Solution:**



$$\frac{p_A}{\gamma} + z_A + \frac{V_A^2}{2g} = \frac{p_B}{\gamma} + z_B + \frac{V_B^2}{2g}$$

$$\frac{p_A}{\gamma} = \frac{V_B^2}{2g}$$

$$V_B = \sqrt{2 \frac{p_A}{\rho}} = \sqrt{2 * 75000 / 999} = 12.3 \text{ m/s}$$

$$\sum F_x = \frac{d}{dt} \int_{CV} u \rho dV + \int_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$-F = \sum_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$= V \rho (-VA)$$

$$F = \rho Q V = 999 * 0.4 * 12.3 = 4.9 \text{ kN}$$

Example

- **Given:** Figure
- **Find:** External reactions in x and y directions needed to hold fixed vane.
- **Solution:**

$$\sum F_x = \frac{d}{dt} \int_{CV} u \rho dV + \int_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$F = \sum_{CS} u \rho \vec{V} \cdot \vec{A}$$

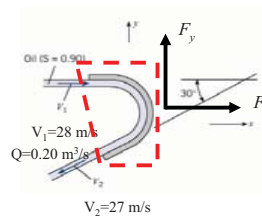
$$= V_1 \rho (-V_1 A) + (-V_2 \cos 30^\circ) \rho (V_2 A_2)$$

$$F = -V_1 \rho (V_1 A_1) - V_2 \cos 30^\circ \rho (V_2 A_2)$$

$$= -\rho Q (V_1 + V_2 \cos 30^\circ)$$

$$= -0.9 * 1000 * 0.2 (28 + 27 \cos 30^\circ)$$

$$F_x = -9.25 \text{ kN (to the left)}$$



Example

$$\sum F_y = \frac{d}{dt} \int_{CV} v \rho dV + \int_{CS} v \rho \vec{V} \cdot \vec{A}$$

$$F_y = \sum_{CS} v \rho \vec{V} \cdot \vec{A}$$

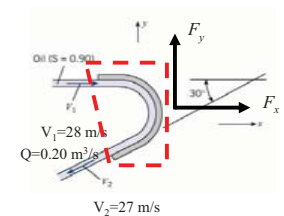
$$= (-V_2 \sin 30^\circ) \rho (V_2 A_2)$$

$$F = -V_2 \sin 30^\circ \rho (V_2 A_2)$$

$$= -\rho Q (V_2 \sin 30^\circ)$$

$$= -0.9 * 1000 * 0.2 (27 \sin 30^\circ)$$

$$F_y = -2.43 \text{ kN (down)}$$



Example

- Given:** Figure
- Find:** Force applied to flanges to hold pipe in place
- Solution:** Continuity equation

$$Q = V_1 A_1 = V_2 A_2$$

$$V = Q / A = 0.6 / (\pi * 0.3^2 / 4) = 8.49 \text{ m/s}$$

- Momentum**

$$\Sigma F_x = \frac{d}{dt} \int_{CV} u \rho dV + \int_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$F_x + p_1 A_1 + p_2 A_2 = V_1 \rho (-V_1 A_1) - V_2 \rho (V_2 A_2)$$

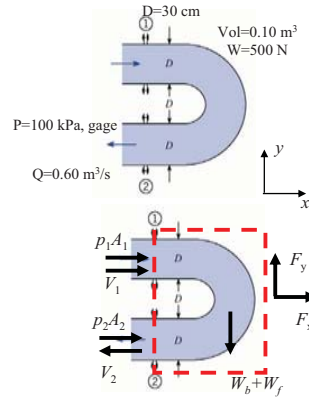
$$F_x = -2(100,000)(\pi * 0.3^2 / 4) - 2 * 8.49 * 1000 * 0.6$$

$$F_x = -24,325 \text{ N}$$

$$\Sigma F_y = \frac{d}{dt} \int_{CV} v \rho dV + \int_{CS} v \rho \vec{V} \cdot \vec{A}$$

$$F_y - W_b - W_f = 0$$

$$F_y = 500 + 0.1 * 9810 = 1481 \text{ N}$$



Example

- Given:** Water jet, 6 cm diameter, with velocity 20 m/s hits vane moving at 7 m/s.
- Find:** Find force on vane by water.
- Solution:** Select CV moving with the vane at constant velocity. The magnitude of the velocity along the vane is constant

$$V_1 = V_2 = V - V_v$$

$$V_1 A_1 = V_2 A_2 = (V - V_v) A$$

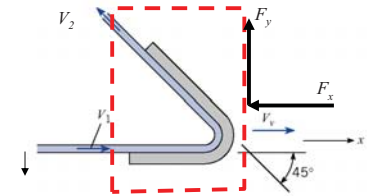
$$\Sigma F_x = \frac{d}{dt} \int_{CV} u \rho dV + \int_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$-F_x = (V - V_v) \rho [-(V - V_v) A_1] + (V - V_v) \cos 45^\circ \rho [(V - V_v) A_2]$$

$$= -(V - V_v)^2 \rho A (1 + \cos 45^\circ)$$

$$= -(20 - 7)^2 (1000)(\pi * 0.06^2 / 4)(1 + \cos 45^\circ)$$

$$F_x = 815.7 \text{ N}$$



$$\Sigma F_y = \frac{d}{dt} \int_{CV} v \rho dV + \int_{CS} v \rho \vec{V} \cdot \vec{A}$$

$$F_y = (V - V_v) \sin 45^\circ \rho [(V - V_v) A_2]$$

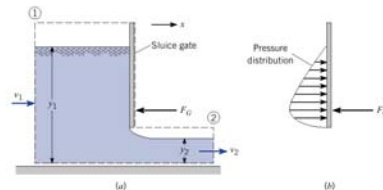
$$= (V - V_v)^2 \rho A \sin 45^\circ$$

$$= (20 - 7)^2 (1000)(\pi * 0.06^2 / 4)(\sin 45^\circ)$$

$$F_y = 337.9 \text{ N}$$

Sluice Gate

- Find:** Force due to pressure on face of gate
- Solution:**
Assume: v_1 and v_2 are uniform (so pressure is hydrostatic)



$$\Sigma F_x = \frac{d}{dt} \int_{CV} u \rho dV + \int_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$\Sigma F_x = v_1 \rho [-v_1 A_1] + v_2 \rho [v_2 A_2]$$

$$\bar{p}_1 A_1 - \bar{p}_2 A_2 - F_G = \rho Q (v_2 - v_1)$$

$$(\gamma \frac{y_1}{2} y_1 b) - (\gamma \frac{y_2}{2} y_2 b) - F_G = \rho Q (v_2 - v_1)$$

$$F_G = \rho Q (v_1 - v_2) + \frac{\gamma b}{2} (y_1^2 - y_2^2)$$

Exercise:

5.14, 5.29, 5.31, 5.50, 5.52, 5.56

Continuity Equation

- Reynolds Transport Theorem

$$B = M_{sys} \text{ (extensive)}$$

$$b = \frac{dB}{dm} = \frac{dM_{sys}}{dm} = 1 \text{ (intensive)}$$

$$\frac{dB_{sys}}{dt} = \frac{d}{dt} \int_{CV} b \rho dV + \sum_{CS} b \rho \vec{V} \cdot \vec{A}$$

$$0 = \frac{d}{dt} \int_{CV} \rho dV + \sum_{CS} \rho \vec{V} \cdot \vec{A}$$

Unsteady Case

$$0 = \sum_{CS} \rho \vec{V} \cdot \vec{A}$$

Steady Case

1-D Flow in a Conduit

- Continuity Eq.

$$0 = \frac{d}{dt} \int_{CV} \rho dV + \sum_{CS} \rho \vec{V} \cdot \vec{A}$$

- Steady flow

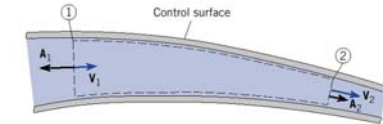
$$0 = \sum_{CS} \rho \vec{V} \cdot \vec{A}$$

- Incompressible fluid

$$0 = -V_1 A_1 + V_2 A_2$$

$$V_1 A_1 = V_2 A_2$$

$$Q_1 = Q_2$$



Momentum Equation

- Reynolds Transport Theorem

$$\frac{dB_{sys}}{dt} = \frac{d}{dt} \int_{CV} b \rho dV + \int_{CS} b \rho \vec{V} \cdot \vec{A}$$

- b = velocity; B_{sys} = system momentum

$$\sum \vec{F} = \frac{d}{dt} \int_{CV} \vec{V} \rho dV + \int_{CS} \vec{V} \rho \vec{V} \cdot \vec{A}$$

- Vector equation -- 3 components, e.g., x

$$\sum F_x = \frac{d}{dt} \int_{CV} u \rho dV + \int_{CS} u \rho \vec{V} \cdot \vec{A}$$

$$\frac{dB_{sys}}{dt} = \frac{d\vec{M}_{sys}}{dt} = \sum \vec{F}$$

$$\vec{V} = u\vec{i} + v\vec{j} + w\vec{k}$$